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Description

This invention relates to the polymerization of tetrafluoroethylene (TFE) monomer with perfluoro(alkyl vinyl ether) monomer (PAVE) in a perfluorinated or partially fluorinated fluorocarbon solvent in the presence of an alkane (C₁-C₃) chain transfer agent.

Prior to this invention, TFE and PAVE monomers have been polymerized in the above-mentioned fluorocarbon solvents using, for example, methanol as chain transfer agent (see US-A-3 642 742). A chain transfer agent is desirable in the type of TFE polymerization described herein to alter the end groups of the resulting melt-processible TFE/PAVE copolymers and control molecular weight and molecular weight distribution. Without use of a chain transfer agent, said end groups tend to be unstable ones, such as -COF, -COOH and -CF=CF₂. On subjecting copolymers with these end groups to heat, the end groups tend to decompose or rearrange with release of gases such as CO₂ and/or HF. These gases cause bubbles in molded copolymer parts and, in addition, the HF is highly corrosive.

Methanol as a chain transfer agent has not been ideal. Methanol tends to be recycled with monomer, and it is difficult to sample and analyze for methanol when mixed with monomer. Therefore, it is hard to know how much methanol to add to the polymerization vessel to achieve the desired effect. In addition, the methanol acts to solubilize transient water and HF in the system, which results in corrosion of the polymerization equipment. Moreover, the methanol forms -CH₂OH end groups in the copolymer which are themselves subject to attack by oxygen at extrusion temperatures with both release of HF and conversion of the -CH₂OH end groups to unstable -COF end groups.

It has now been found that use of a C₁ to C₃ alkane as the chain transfer agent in place of methanol overcomes many of the problems associated with methanol while maintaining desirable molecular weight and molecular weight distribution control.

Use of a C₁ to C₃ alkane, i.e. methane, ethane or propane, has been found to have several advantages. For example, alkane concentration in the process can be controlled more effectively than methanol because alkanes can be more readily analyzed when mixed with monomer. The alkanes produce -CH₃ end groups, which are more thermally stable than -CH₂OH groups. They are less corrosive due to the lower solubility of water and HF in the solvent. Finally, the C₁-C₃ alkanes aid in producing polymers of narrow molecular weight distribution index which is desirable in some end uses. This feature is unique when compared with a variety of other hydrocarbon chain transfer agents.

Specifically, this invention is a process for making a melt-processible tetrafluoroethylene copolymer which comprises polymerizing tetrafluoroethylene with at least one perfluoro(alkyl vinyl ether) comonomer of the formula R_fO-CF=CF₂ wherein R_f is perfluoroalkyl of 1-6 carbon atoms, in a liquid organic solvent selected from perfluorinated solvents and chlorofluoroalkane solvents in which each carbon atom has at least one fluorine atom attached thereto, at a temperature of between 30° C and 75° C and a pressure of between 0.1 and 6.9 MPa gauge (15 and 1000 psig) in the presence of a polymerization initiator and in the presence of a chain transfer agent wherein the chain transfer agent is methane, ethane, or propane. The resulting polymer can then be melt-shaped as desired.

The polymerization of tetrafluoroethylene with perfluoroalkyl vinyl ether comonomer is well known, having been described in a number of patents, such as US-A-3,642,742, which describes such polymerization being carried out in an organic liquid medium in the presence of certain chain transfer agents. The present invention involves the same process but uses a different chain transfer agent.

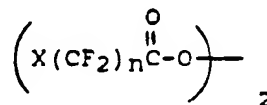
Suitable solvents for the process are perfluorinated solvents such as perfluorocyclobutane, perfluorodimethyl cyclobutane and perfluorocyclohexane. Preferred solvents are commercially available chlorofluoroalkanes and some chlorofluorohydroalkanes, having from 1-4 carbon atoms and preferably 1-2 carbon atoms in which each carbon atom is substituted by at least one fluorine atom. Said chlorofluoroalkanes may also contain a maximum of one hydrogen atom per carbon atom if the hydrogen is present only in the difluoromethyl grouping (-CF₂H). Suitable solvents should be liquid at polymerization conditions. Examples of preferred solvents are as follows: CCl₂F₂, CCl₃F, CClF₂H, CCl₂FCCl₂F, CCl₂FCClF₂ and CClF₂CClF₂. These compounds are sold under the trade names "Freon" 12, "Freon" 11, "Freon" 22, "Freon" 112, "Freon" 113 and "Freon" 114, respectively. The most preferred solvent is "Freon" 113.

One or more comonomers are copolymerized or terpolymerized with tetrafluoroethylene to produce a co- or ter-polymer.

Monomers which can be used are the perfluoro(alkyl vinyl ethers) having the general formula CF₃(CF₂)_nOCF=CF₂ where n is a cardinal number of 1-5, such as perfluoroethyl perfluorovinyl ether and perfluoropropyl perfluorovinyl ether.

Any suitable initiator for TFE nonaqueous polymerization can be used. It should be soluble in the fluorocarbon solvents, have high activity between 30° C and 75° C and be substantially nontelogenic. Also,

the initiators must give radicals which will result in stable end groups on the polymer chain. Fluorocarbon acyl peroxides are suitable initiators. Fluorocarbon acyl peroxides which are suitable for use in the process are represented by the formula



where X=H, Cl or F and n=1-10. The preferred initiator is bis(perfluoropropionyl) peroxide. A low temperature initiator must be used because the temperature of the polymerization system should not go over 75°C. Above 75°C, the rearrangement of the perfluorovinyl ether occurs so much more rapidly that a greater number of chains are terminated in acid fluoride end groups than is normally desirable.

Carboxylic acid end groups in the polymer are termed "unstable end groups" because they decompose readily during fabrication of the polymer, giving rise to bubbles in the finished product. Other end groups such as vinyl and acid fluoride end groups are also included in the category of unstable end groups because they are readily converted to carboxylic acid end groups.

The existence and quantity of these end groups can be determined by the infrared spectrum generally obtained on compression molded films of about 0.25 mm (10 mils) thickness.

The term "specific melt viscosity" as used herein means the apparent melt viscosity as measured at 372°C under a shear stress of 6.5 pounds per square inch (45 kPa). Specific melt viscosity is determined by using a melt indexer of the type described in ASTM D-1238-52-T, modified for corrosion resistance by employing a cylinder, orifice, and a piston made of Stellite cobalt-chromium-tungsten alloy. The resin is charged to the 0.375 inch (.95 cm) I.D. cylinder which is held at 372°C ± 0.5°C, allowed to come to an equilibrium temperature during 5 minutes, and extruded through the 0.0825 inch (2 mm) diameter, 0.315 inch (8 mm) long orifice under a piston loading of 5000 grams. The specific melt viscosity in 0.1 Pas (poises) is calculated as 53,150 divided by the observed extrusion rate in grams per minute.

The specific melt viscosity of the copolymers will be below 1 x 10⁶ Pas (1 x 10⁷ poise) at 372°C to insure the melt-processible character of the product. The resulting copolymers are non-elastomeric and are useful as films, fibers and tubes for example.

As the examples will show, the melt viscosity and the molecular weight distribution index of the copolymers produced are very close to those of the same copolymer produced using methanol as chain transfer agent, thus showing that the C₁-C₃ alkanes are just as effective in terms of these criteria.

Moreover there were no unstable -CH₂OH end groups in the polymer so made and only the expected number of -COF end groups (or COOH groups resulting from hydrolysis of -COF groups) from comonomer rearrangement were present. Most importantly, there was no change during extrusion of the number of -COF end groups present, which means that little, if any, HF was produced.

Molecular Weight Distribution Index (MWDI) is defined as MV₁₀/MV₅. MV₅ is the apparent melt viscosity in a high temperature melt viscometer, such as that made by F. F. Slocomb Co., Wilmington, DE. MV₅ is based on melt flow rate using 5000 g total mass while urging the melt through the orifice. The sample is kept in the viscometer at 372°C for 5 minutes before the flow is measured.

MV₁₀ is measured after MV₅, and is the melt flow rate using 833 g total mass, starting the measurement 10 minutes after the sample entered the viscometer.

The PPVE content of a copolymer is measured using infrared spectrometry on a compression molded film using absorbance at 993 cm⁻¹ as a measure of PPVE content and absorbance at 2353 cm⁻¹ as a measure of sample thickness. The ratio A₉₉₃:A₂₃₅₃ is related to PPVE content of the polymer by means of a calibration curve using known copolymers. F₁₉ NMR is used as the primary standard for calibrating the reference films.

EXAMPLES

Comparison Experiment 1

Experiment Using Methanol as Chain Transfer Agent

Into an evacuated, one liter, stainless steel, agitated pressure vessel were charged 830 ml of 1,2,2-trichloro-1,1,2-trifluoroethane ("Freon" 113), 30.6 grams perfluoropropyl-perfluorovinyl ether (PPVE), and 0.38 g methanol. The mixture was heated to 60°C and tetrafluoroethylene (TFE) was charged into the

TABLE I

TFE/PPVE POLYMERIZATIONS WITH HYDROCARBON CHAIN TRANSFER AGENTS

POLYMERIZATIONS: 15 MINUTES/60°C/0.09 G TOTAL 3P INITIATOR

Comparison Sample Number	ML F-113	PPVE Grams	Chain Transfer Agent (CTA)	M_n CTA Grams	TFE Clave (PSIG)	Yield Grams	M_w (10 ⁻⁴) Polise)	MWDI %	PPVE % wt	End Groups Number/10 ⁶ CS -COF -COOH
2	820	30.6	Cyclopropane	1.74	0.47 (67)	42.7	43	3.7	3.90	40 18
3	820	30.6	Butane	0.09	0.47 (67)	35.5	9.2	6.0	4.08	95 0
4	840	30.6	t Butyl Cyclohexane	0.20	0.47 (66)	32.8	30	8.3	3.28	38 10
5	835	30.6	Norborane	0.075	0.47 (66)	34.1	34	6.3	3.30	33 33
6	820	30.6	Adamantane	0.10	0.47 (66)	25.6	2.0	8.4	3.50	48 40
7	820	30.6	Cyclohexane	0.10	0.47 (66)	32.4	5.5	4.3	3.10	NM NM
8	840	30.6	Cyclopentane	0.15	0.47 (66)	28.5	4.2	7.2	2.95	43 0
9	840	30.6	n-Hexane	0.10	0.47 (66)	26.0	28.3	11.0	3.39	0 70
10	840	30.6	n-Pentane	0.10	0.47 (66)	25.7	27.3	4.5	2.98	37 31

NM = not measured

55 Claims

1. A process for making a melt-processible tetrafluoroethylene copolymer with comprises polymerizing tetrafluoroethylene with at least one perfluoro(alkyl vinyl ether) comonomer of the formula $R_1O-CF=CF_2$

wherein R_1 is perfluoroalkyl of 1-6 carbon atoms, in a liquid organic solvent selected from perfluorinated solvents and chlorofluoroalkane solvents in which each carbon atom has at least one fluorine atom attached thereto, at a temperature of between 30 °C and 75 °C and at a pressure of between 0.1 and 6.9 MPa gauge (15 and 1000 psig) in the presence of a polymerization initiator and in the presence of a chain transfer agent, characterized in that the chain transfer agent is methane, ethane or propane.

2. A process according to Claim 1 wherein the liquid organic solvent is at least one of CCl_2F_2 , CCl_3F , $CClF_2H$, CCl_2FCCl_2F , CCl_2FCClF_2 and $CClF_2CClF_2$, and the chain transfer agent is ethane.
3. A process according to Claim 1 or 2 wherein the comonomer is perfluoro(propyl vinyl ether).
4. A process according to Claim 3 wherein the solvent is CCl_2FCClF_2 .
5. A process according to any one of the preceding claims which comprises the additional step of melt-shaping the resulting copolymer.

Revendications

1. Un procédé pour fabriquer un copolymère de tétrafluoréthylène façonnable à l'état fondu, qui consiste à polymériser du tétrafluoréthylène avec au moins un comonomère qui est un perfluoro(éther d'alkyle et de vinyle) de la formule $R_1O-CF=CF_2$ où R_1 est un groupe perfluoroalkyle de 1 à 6 atomes de carbone, dans un solvant organique liquide choisi parmi les solvants perfluorés et les solvants du type chlorofluoroalcane dans lesquels au moins un atome de fluor est fixé à chaque atome de carbone, à une température comprise entre 30 °C et 75 °C et sous une pression comprise entre 0,1 et 6,9 MPa au manomètre (15 et 1000 psig), en présence d'un initiateur de polymérisation et en présence d'un agent de transfert de chaîne, caractérisé en ce que l'agent de transfert de chaîne est le méthane, l'éthane ou le propane.
2. Un procédé selon la revendication 1, dans lequel le solvant organique liquide est l'un au moins de CCl_2F_2 , CCl_3F , $CClF_2H$, CCl_2FCCl_2F , CCl_2FCClF_2 et $CClF_2CClF_2$, et l'agent de transfert de chaîne est l'éthane.
3. Un procédé selon la revendication 1 ou 2, dans lequel le comonomère est le perfluoro(éther de propyle et de vinyle).
4. Un procédé selon la revendication 3, dans lequel le solvant est CCl_2FCClF_2 .
5. Un procédé selon l'une quelconque des revendications précédentes, qui comprend l'étape supplémentaire de façonnage à l'état fondu du copolymère résultant.

Patentansprüche

1. Verfahren zur Herstellung eines schmelzverarbeitbaren Tetrafluorethylencopolymeren, bei dem Tetrafluorethylen mit mindestens einem Perfluor(alkylvinylether)-Comonomeren der Formel $R_1O-CF=CF_2$, worin R_1 Perfluoralkyl von 1-6 Kohlenstoffatomen ist, in einem flüssigen organischen Lösungsmittel, ausgewählt aus perfluorierten Lösungsmitteln und chlorfluoralkanlösungsmitteln, in denen jedes Kohlenstoffatom mindestens ein daran gebundenes Fluoratom hat, bei einer Temperatur zwischen 30 °C und 75 °C und einem Druck zwischen 0,1 und 6,9 MPa Manometerdruck (15 und 1000 psig) in Gegenwart eines Polymerisationsinitiators und in Gegenwart eines Kettenübertragungsmittels polymerisiert wird, dadurch gekennzeichnet, dass das Kettenübertragungsmittel Methan, Ethan oder Propan ist.
2. Verfahren nach Anspruch 1, worin das flüssige organische Lösungsmittel mindestens eines von CCl_2F_2 , CCl_3F , $CClF_2H$, CCl_2FCCl_2F , CCl_2FCClF_2 und $CClF_2CClF_2$ und das Kettenübertragungsmittel Ethan ist.
3. Verfahren nach Anspruch 1 oder 2, bei dem das Comonomere Perfluor(propylvinylether) ist.
4. Verfahren nach Anspruch 3, worin das Lösungsmittel CCl_2FCClF_2 ist.

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5. Verfahren nach einem der vorhergehenden Ansprüche mit dem zusätzlichen Schritt der Schmelzverformung des erhaltenen Copolymeren.

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